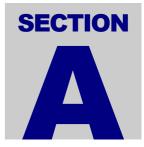
# Form C gas

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## **A1 PRINCIPAL SHIP PARTICULARS**

1.1	Name of Ship	KING ARTHUR
1.2	Previous Name(s)	n/a
1.3	Builder	Vinashin - Bachdang
1.4	Date of delivery	2 / 2011
1.5	Classification Society and No. RINA /	R.I.NA RI 85529
1.6	Gross Registered Tonnage	4.761
1.7	Net registered Tonnage	1.428
1.8	Suez Tonnage Gross/Net	5506,53 / 4086,11
1.9	Panama tonnage Gross/Net	Not yet calculed
1.10	Registered Owner	Mediterranea di Navigazione S.p.A.
	Address	P.zza Caduti sul Lavoro, 3 – 48122 Ravenna - Italy
	Telephone	+39 0544 598911
	Telex/fax	+39 0544 423799
1.11	Manager or Operator	Mediterranea di Navigazione S.p.A.
	Address	P.zza Caduti sul Lavoro, 3 – 48122 Ravenna - Italy
	Telephone	+39 0544 598911
	Telex/fax	+39 0544 423799
1.12	Flag	Italian –
1.13	Port of registry	Ravenna
1.14	Official No.	52 R.I.
1.15	Call Sign	IBAI
1.16	Immarsat No.	00870 - 773141203
1.17	LR/IMO No.	9480382
1.18	Was the ship built in accordance with the	e following regulations
	IMO	Yes
	USCG	Yes
	RINA	Yes
	OTHER	Yes
1.19	IMO Certification	
	Certificate of Fitness IGC	
	A328	
	A329	
	Letter of Compliance	
1.20	Date questionnaire compiled	06.10.2017

# **A2 HULL DIMENSIONS**

2.1	Length overall	104 m.
2.2	Length between perpendiculars	97.20 m
2.3	Extreme breadth	16.40 m.
2.4	Extreme depth	8,4 m
2.5	Summer draught	7 <b>,</b> 2 m
2.6	Corresponding deadweight	5.312 tonn
2.7	Light displacement	3.043 tonn
2.8	Load displacement (summer)	8.355 tonn
2.9	Cargo tank cubic capacity (100%)	4655.83 cbm
2.10	Distance from keel to top antenna	32.5 m
2.11	Air draught (with normal ballast)	27.5 m

### **A3 BALLAST PARTICULARS**

- 3.1 Permanent Ballast No
- 3.2 Ballast quantity
- 3.3 Bunkers, stores, etc. Fuel 428 t;3.4 Draught Forward

- Forward - Aft

- Aft - Mean

5,0 m

2.000 t abt.

4,50 m

5.50 m

Diesel 101 t ;Oils 29 t ;Misc. 0 t;Fresh Water 0 t;Water 122 t

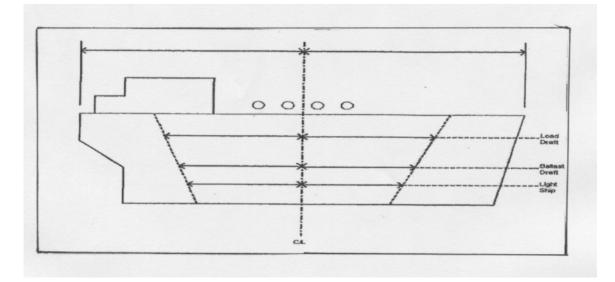
#### **A4 IMMERSION**

4.1	TPC at normal ballast draught	12,80 t/cm
4.2	TPC at loaded draught	14,50 t/cm

### **A5 LOADED PARTICULARS**

5.1	Cargo	ETHYLENE	BUTANE	PROPANE	V.C.M.
5.2	Density	0.569 t/m3	0.600 t/m3	0.583 t/m3	0.972 t/m3
5.3	Cargo tons	2611	2748	2670 t	4364 t
5.4	Bunkers IFO	428 t	428 t	428 t	424 t
5.5	GASOIL	101 t	101 t	101 t	101 t
5.6	Fresh water	0 t	0 t	0 t	0 t
5.7	Stores/spares	40 t	40 t	40 t	40 t
5.8	Lub oil (at 95% + bilge/sludge)	29 t	29 t	29 t	29 t
5.9	Ballast	569	506 t	504 t	359 t
5.10	Deadweight	3900 t	3975 t	3895 t	5440 t
5.11	Draught - Forward	5.328 m	5.402 m	5.352 m	6.877 m
	- Aft	6.870 m	6.951 m	6.901 m	7.522 m
	- Mean	6.099 m	6.154 m	6.122 m	7.200 m

## **A6 PARALLEL MID-BODY DIMENSIONS**



Distance bow to mid-point manifold: 58,3 m. Distance stern to mid-point manifold: 45,6 m . Light ship parallel body length: 47,5 m Light ship parallel body – bow to mid-point manifold: 24,2 m Light ship parallel body – stern to mid-point manifold: 23,3 m Normal ballast parallel body length: 54,3 m abt. Normal ballast parallel body length – bow to mid – point manifold: 27 m Normal ballast parallel body length – stern to mid – point manifold: 27,3 m Parallel body length at SUMT – bow to manifold: 28 m Parallel body length at SDWT – stern to mid – point manifold: 28,3 m

## **A7 BUNKER CAPACITIES**

7.1	M.E. Fuel Oil	Grade	
		Capacity 98%	432 cbm
7.2	Diesel Oil Grade		
		Capacity 98%	121 cbm

## **A8 FUEL CONSUMPTION DETAILS**

8.1	At sea (normal service speed)	IFO 380 - 15,5 tonn / day
8.2	At sea (normal service speed) while conditioning cargo	IFO 380 – 15,5 tonn / day
8.3	In port, loading	3,5 tonn / day
8.4	In port, discharging	<b>4,6 tonn / day</b>
8.5	In port, idle	2,1 tonn / day

## **A9 MAIN ENGINE PARTICULARS**

9.1	Main engine make and type		WARTSILA TYPE 8L32
9.2 No	o. of units		1
9.3	Maximum continuous rating per engine	(MCR)	4000 kW - 750 RPM
9.4	Total available power		CSR
9.5	Normal service power (ECR)		CSR – 3400 kW

# A10 AUXILIARY PLANT

10.1	Make and type generators	of auxiliary	VOLVO PENTA TYPE D16
10.2	No. of units		4
10.3	Maximum generator	output per	470 kWe
	unit		
10.4	Shaft generator		1600 kWe – MARELLI (WARTSILA)
10.5	Emergency generator		MAKE STX Eng. Co KOREA – 90 kW
10.6	Total available power		3480 kWe
	_		

## **A11 POWER/SPEED INFORMATION**

11.1	Trial data	BHP
		MCR
		Speed
		Draught
11.2	Normal service s	speed BHP
		MCR

MCR Speed Draught

## **A12 THRUSTERS**

- 12.1 Make and type
- 12.2 No. Installed

THRUSTMASTER&SAM ELETRONICS - 400 kW

12.3 Location and rated bollard pull

#### **A13 FRESH WATER**

13.1	Capacity of distilled tanks	9.10 cbm
13.2	Capacity of domestic tanks	115.11 cbm
13.3	Daily consumption distilled	8.05 cbm
	domestic	
13.4	Daily evaporator production	10 t/day

#### A14 BALLAST CAPACITIES AND PUMPS

1

Abt fr. 131

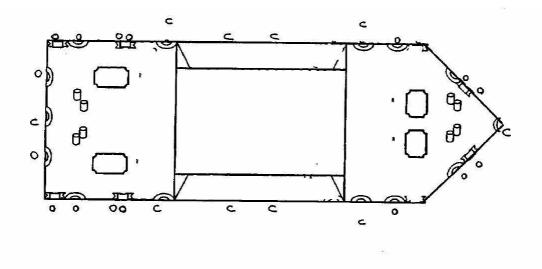
#### Fill the following table

		Tank	Capacity	CBM	CBM
14.1		Fore peak	136		
14.2		Wing or side tanks	1899		
14.3		Double bottoms	n/a		
14.4		Aft peak	18		
14.5		Other ()	n/a		
14.6		Total	2054		
14.7	Ballast pump make and type	GARBARINO – TYPE MU150-315LE			
14.8	No. of Pumps	2 (N° 1 Service; N° Spare)			
14.9	Total capacity	2 x 460 cbm/H x 30 m.w.l			
14.10	Location	Engine Room			
14.11	Control Location	C.C.R./Locally			

#### **A15 MOORING EQUIPMENT**

15.1 Ropes and Wires.

On the diagram below indicate the position of winch mounted ropes (R) together with open (O) and (Panama) closed (C) fairleads.



#### 15.2 Mooring Winches

		No	Motive power (steam,hydraul)	Heaving power	Brake Capacity	Hauling speed
Forecast	le	2	hydraulic	tbd	27 t	12 m/min
Poop		2	hydraulic	tbd	27 t	12 m/min
15.3	Anchors and Windlasses	2				
	Windlass motive Power (steam, hydraulic)	hydraulic				
	Hauling power	tbd				
	Brake holding capacity	24.6 t				
	Anchor type	HHP ANCH	IOR BALANCED			
	Weight	2295 kg				
	Is spare carried	No				
	Cable diameter	44 mm				
	No of schackles port					
	No of schackles starboard					
15.4	Windage					
	Windage on ballast draught					
	Windage full loaded					

# A16 NAVIGATIONAL EQUIPMENT

Is the following equipment fitted :

16.1	Magnetic compass	YES
16.2	Gyro compass and repeaters	YES
16.3	Radars	YES
16.4	Radar plotting equipment	YES
		YES
16.5	Arpa	
16.6	Echo sounder	YES
16.7	Speed/Distance indicator	YES
16.8	Doppler log	YES
16.9	Rudder angle, RPM, controllable pitch and	YES
	Thrusters indicators	
16.10	Rate of turn indicator	tbd
		YES
16.13	Satellite navigator	YES
16.14	Decca navigator	NO
16.15	Loran C	NO
16.16	Sextants	YES
16.17	Signal lamp (aldis)	YES
16.18	Course recorder	YES
16.19	Engine order printer	YES
16.20	What chart outfit coverage is provided if limited, indicate	
areas co	0 1	
areas co	wered	

16.21 Formal chart correction system in use

# **A17 COMMUNICATION EQUIPMENT**

Is the following equipment fitted :

17.1	Is ship with GMDSS YES	Yes
17.2	Radio telegraph main transmitter including facility to	Yes
	transmit on radio telephone distress frequency YES	
17.3	Radio telegraph main receiver including facility to receive on	Yes
	radio telephone distress frequency YES	
17.4	Radio telephone distress frequency watch receiver YES	Yes
17.5	Main radio antenna YES	Yes
17.6	Radio telegraph reserve transmitter	n/a
17.7	Radio telegraph reserve receiver	n/a
17.8	Reserve radio antenna	Yes
17.9	Are the main and reserve installation electrically separate and	Yes
	electrically independent of each other	
17.10	Radio telegraph auto alarm	NO
17.11	2182 KHZ bridge watch receiver	NO
17.12	Alarm signal generating device	YES
17.13	VHF radio	YES
17.14	Inmarsat satellite communications system	YES
	if yes, state identification number	00870 773141203
17.15	Telex	YES
	if yes, state identification number	0580 424729315/20
17.16	Telefax	YES
	if yes, state identification number	00870 783140831
17.17	Weatherfax	YES
17.18	Epirbs	YES
17.19	At least three survival craft two-way radio telephone	YES
	apparatus	
17.20	Emergency lifeboat transmitter	YES
17.21	Full set of publications	YES
17.22	Satellite Epirb	YES
17.23	VHF Epirb	NO
17.24	Radio transponder for survival craft	YES



## **B1 CARGO - GENERAL INFORMATION**

1.1 List products which the ship is certified to carry

Acetaldehyde Anhydrous Ammonia Butadiene Butanes (iso and normal) Butylenes Butane / Propane Mixtures Propane Commercial Propane (max. Ethane in liquid phase 2.5 mol. %) Propylene Vinyl Chloride Monomer Isoprene Ethane Butadiene and C4 Hydrocarbon Mixtures Ethylene -104 °C

8.0 Barg IMO (6 Barg USCG)

- 1.2 Minimum allowable tank temp.
- 1.3 Maximum permissible tank pressure
- 1.4 List grades which can be transported simultaneously

Acetaldehyde Anhydrous Ammonia Butadiene Butanes (iso and normal) Butylenes Butane / Propane Mixtures Propane Commercial Propane (max. Ethane in liquid phase 2.5 mol. %) Propylene Vinyl Chloride Monomer Isoprene Ethane Butadiene and C4 Hydrocarbon Mixtures Ethylene

1.5 List grades which can be loaded or discharged simultaneously

> Acetaldehyde Anhydrous Ammonia Butadiene Butanes (iso and normal) Butylenes Butane / Propane Mixtures Propane Commercial Propane (max. Ethane in liquid phase 2.5 mol. %) Propylene Vinyl Chloride Monomer Isoprene Ethane Butadiene and C4 Hydrocarbon Mixtures Ethylene

1.6 State natural tank segregation. (N.B. separation obtained by the removal of spools or by insertion of blind flange)

2 (by spool pieces removal)

#### CARGO SYSTEMS

1.7 Number of products, (gas) that can be conditioned by reliquefaction **2 (two)** simultaneously.

## **B2 CARGO TANKS**

2.1	No. and type of cargo tanks	2 (two indep
2.2	Maximum allowable relief valve setting	8.0 Barg
2.3	Safety valve set pressure - if variable give range for pilot valve	8.0 Barg (IN 6.0 Barg (US
2.4	Maximum vacuum	0.75 Bar abs
2.5	Maximum cargo density	970 kg/m <sup>3</sup>
2.6	Maximum rate of cool-down	
2.7	State any limitations regarding partially	

- 2.7 State any limitations regarding partially filled tanks
- 2.8 State allowable combinations of filled and empty tanks

(two independent Type C)

8.0 Barg (IMO Setting) 6.0 Barg (USCG Setting) 0.75 Bar absolute 970 kg/m<sup>3</sup>

# **B3 CARGO TANK CAPACITIES**

Complete the following table

TANK	Capacity CBM	Capacity CBM	PROPANE	AMMONIA	BUTANE	VCM
	100%	98%	Tonnes -42.8°C	Tonnes -33°C	Tonnes -0,5°C	Tonnes -13,4°C
1	2157	2114	1231	1441	1273	2043
2	2374	2326	1355	1586	1401	2249
3						
4						
5						
6						
TOTALS						

#### **B4 LOADING RATES**

		PRODUCT	RATE (Cbm	ı/hr)
4.1	From refrigerated storage		With vapour return	Without return
4.2		BUTANE	400	400
4.3		PROPANE	400	<b>400</b>
4.4		AMMONIA	400	<b>400</b>
4.5		ETHYLENE	400	<b>400</b>
4.6				
4.7				
		PRODUCT	RATE (Cbr	ı/hr)
4.8	From pressure storage		With vapour return	Without return
4.9		BUTANE 0-30°C	350	300/250
4.10		PROPANE 0°C	350	200
4.11		10° C	350	150
4.12		20° C	350	120
4.13		30° C	350	100

# **B5 DISCHARGING - GENERAL**

Cargo	pumps	
5.1	Type of pumps	Centrifugal Deepwell Pump
5.2	Number per tank	<b>1</b> (one)
5.3	Rate (per pump)	400 m <sup>3</sup> /hr
5.4	Delivery head	120 m.l.c.
5.5	Maximum density	0.972 kg/l
	Booster pumps	
5.6	Type of pump	Centrifugal Pump (Horizontal)
5.7	Number	<b>1</b> (one)
5.8	Rate (per pump)	400 m <sup>3</sup> /hr
5.9	Delivery head	120 m.l.c.
5.10	Maximum density	0.69 kg/l
		-

## **B6 DISCHARGE PERFORMANCES**

Full cargo discharge times (using all main pumps)

		MANIFOLD	Hou	irs
6.1	From refrigerated	BACK PRESSURE	With vapour return	Without return
6.2		4	4	6
6.3		7	5.5	5.6
6.4		14	11	11
		MANIFOLD	Hou	irs
6.5	Pressurized	MANIFOLD BACK PRESSURE	Hou With vapour return	urs Without return
6.5 6.6	Pressurized			
	Pressurized		With vapour return	Without return

## **B7 UMPUMPABLES**

	TANK NO.	1	2	3	4	5	6	TOTAL TONNES
7.1	Vapour							
7.2	Liquid							
7.3						Total o	quantity	

## **B8 VAPORISING UNPUMPABLES**

8.1	Process used	WARMING
	Time to vaporise liquid unpumpables remaining	ng after full cargo discharge :
8.2	- Propane	2 Hrs
8.3	- Butane	8 Hrs
8.4	- Ammonia	6 Hrs
8.5	- Propylyne	2 Hrs
8.6	-	- hrs
8.7	-	- hrs

## **B9 RELIQUEFACTION PLANT**

9.1 Plant design conditions

	Plant type :		
9.2	Single stage/direct		X 🗌
9.3	Two stage/direct	X 🗌	
9.4	Simple cascade	x 🗆	
9.5	Coolant type	Sea Water / Refrigerant (Propylene)	
	Compressors		
9.6	Туре	BCA - 2K 140-2H	
9.7	Number	2 (two)	
9.8	Capacity (per unit)	40 - 520 kWR	
9.9	Are they oil-free	YES	

## **B10 COOLING CAPACITY**

#### State cooling capacity (in Kcal/hr) for :

10.1	Propane	@-42°C	90283 Kcal/hr
10.2		@ -20°C	171970 Kcal/hr
10.3		@- 5°C	266550 Kcal/hr
10.4	Butane	@- 5°C	171970 Kcal/hr
10.5		@ 0°C	180570 Kcal/hr
10.6		@ 0°C	180570 Kcal/hr

# B11 CARGO TEMPERATURE LOWERING CAPABILITY (AT SEA)

Time taken to lower the temperature of:

11.1	Propane from	+10°C to -42°C	148 Hours
11.2		-5°C to -42°C	131 Hours
11.3		-38°C to -42°C	28 Hours
11.4		+20°C to -0.5°C	21 Hours
11.5		+10°C to -0.5°C	12 Hours
11.6	Butane from	+20°C to -0.5°C	45 Hours
11.7		+ 10°C to -0.5°C	26 Hours
11.8		+10°C to -5°C	43 Hours
11.9	Ethylene from ·	-95°C to -103°C	54 Hours
11.10	Ethylene from -	-98°C to -103°C	<b>37 Hours</b>

# **B12 INERT GAS**

Main inert gas and nitrogen plant

- 12.1 Type of system
- 12.2 Capacity
- 12.3 Composition of inert gas
- 12.4 Dewpoint
- 12.5 Used for
  - Nitrogen
- 12.6 No of bottles
- 12.7 Capacity (each one)
- 12.8 Used for

#### Membrane 450 Nm<sup>3</sup>/hr N2 > 99.0% O2 < 1.0 % Vol. CO2 < 1.0 ppm -55 °C atmospheric Piping flushing and blanketing Cargo Tanks inertization

## **B13 CARGO TANK INERTING/DE-INERTING**

13.1	Time take	n from fresh air to under 5% 02 at -25°C dewpoint
	Time take	n from cargo vapour to fully inert at -25°C dewpoint
13.2	When:	Inert gas density less than product
		Inert gas density greater than product

11 hours 35 hours 35 hours 35 hours

#### **B14 GAS FREEING TO FRESH AIR**

- 14.1 Plant used
- 14.2 Time taken from fully inerted condition to fully breathable fresh air

Cargo compressors

#### 11 hours

# **B15 CHANGING CARGO GRADES**

In this table write down time to change products (in hrs). Write also consumption of nitrogen.

From To	PROPANE TIME/CONS.	BUTANE TIME/CONS.	PROPYLENE TIME/CONS.	AMMONIA TIME/CONS.	VCM TIME/CONS.
PROPANE	TIME/CONS.	21/12	21/12	$\frac{11012}{40/23}$	$\frac{11012}{40/23}$
BUTANE		21/12	21/12	40 / 23	40 / 23
PROPYLENE AMMONIA	21 / 12	40 / 23		85 / 36	40 /23
VCM	40/23	60 / 27	40 / 23	85 / 36	

## **B16 DECK TANK CAPACITY**

16.1	Propane capacity	20 Cbm
16.2	Butane capacity	20 Cbm
16.3	Ammonia capacity	20 Cbm
16.4	Nitrogen capacity	N.A. Ncm

### **B17 PRE-LOADING COOLDOWN**

In the table below, show time and quantity of coolant required to cooldown cargo tanks from ambient temperature and fully gassed up state sufficient to allow loading to commence.

			TIM	E
	PRODUCT	QUANTITY REQUIRED	With return line	Without return
17.1	ETHYLENE	90	12	16
17.2	PROPANE	44	6	8
17.3	BUTANE	15	2	3
17.4	AMMONIA	11	5	6
17.5	VINYL	27	4	5

# **B18 VAPORISER**

- 18.1 Type of vaporiser
- 18.2 Number fitted
- 18.3 Capacity (per unit)
- 18.4 Liquid supply rate
- 18.5 Delivery temperature

### **B19 BLOWER**

- 19.1 Type of blower
- 19.2 Rated capacity
- 19.3 Delivery pressure

Shell and Tube Heat Exchanger 1 (one) 250000 kcal/hr 2000 kg/hr

n.a.

### **B20 CARGO RE-HEATER**

20.1 Type of re-heater

Shell and tube heat exchanger

- 20.2Number fitted120.3Heating mediumSeawater
- Discharge rates with sea water at 15°C to raise product temperature:
- 20.4 for propane from -42°C to -5°C 232 tonnes / hr
- 20.5 for ammonia from -33°C to 0°C 210 tonnes / hr

### **B21 HYDRATE CONTROL**

- 21.1 Freezing point temperature of Depressant
- 21.2 Quantity of Depressant carried
- 21.3 Means of injection

#### **B22 CARGO MEASUREMENT**

LEVEL GAUGES

- 21.1 Are level gauges local or remote
- 21.2 Manufacturer
- 21.3 Туре
- 21.4 Rated accuracy
- 21.5 Certifying authority
- TEMPERATURE GAUGES
- 22.6 Manufacturer
- 22.7 Туре
- 22.8 Rated accuracy
- 22.9 Certifying authority PRESSURE GAUGES
- 22.10 Manufacturer
- 22.11 Type
- 22.12 Rated accuracy
- 22.13 Certifying authority OXYGEN ANALYSER
- 22.14 Manufacturer
- 22.15 Туре

#### FIXED GAS DETECTOR

- 22.16 Manufacturer
- 22.17 Туре
- 22.18 No of points detected PORTABLE GAS DETECTOR
- 22.19 Number
- 22.20 Manufacturer
- 22.21 Type
- TOXIC GAS INDICATOR
- 22.22 Number
- 22.23 Туре
- TOXIC GAS INDICATOR TUBES
- 22.24 Number
- 22.25 Products
- 22.26 Exp.dates
- TANKSCOPE
- 22.27 Type

# **B23 CARGO SAMPLING**

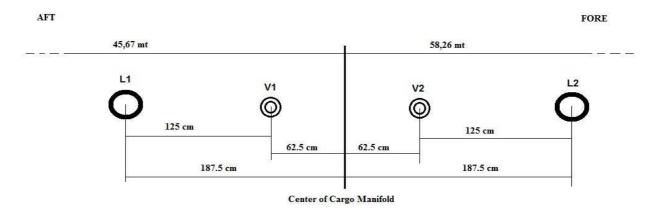
23.1 Fill the following table

	SAI	MPLE	POINTS
CARGO TANKS	TOP	MIDDLE	BOTTOM
1	Yes	Yes	Yes
2	Yes	Ye	Yes
3			
4			
5			
6			
23.2 Can sample be drawn from:			
- Tank vapour outlet			
- Manifold liquid line	Yes		

1	
- Manifold vapour line	Yes
- Pump discharge line	Yes

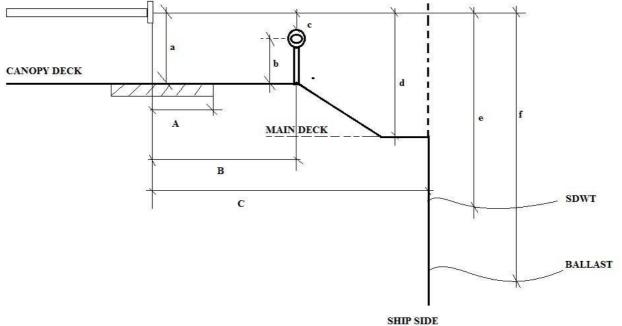
Pump discharge line23.3 State connection type and size

# **B24 CARGO MANIFOLD ARRANGEMENTS**



PIPE FLANGE	DUTY	RATING	SIZE	RAISED ® or Flat (F) face
L1	LIQUID SYSTEM I	ANSI 300	8"	R
V1	VAPOUR SYSTEM I	ANSI 150	4"	R
V2	VAPOUR SYSTEM II	ANSI 150	4"	R
L2	LIQUID SYSTEM II	ANSI 300	8"	R





a)	Spill tank grating to center manifold	1480 mm
b)	Continuous deck to Ship's rail	900 mm
c)	Ship's rail to center manifold (height)	580 mm
d)	Main deck to center manifold	5280 mm
e)	Height of manifold above water line at SDWT	7,68 mt
ſ)	Height of manifold above water line at normal ballast condition	8,58 mt
A)	Distance from manifold to spill tank end	1,50 mt
B)	Distance from manifold to ship's rail (canopy deck)	2,55 mt
Ć)	Distance from manifold to ship's side	<b>3,</b> 70 mt

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### **B25 CARGO MANIFOLD REDUCERS**

0 1 C 1			1 1 1	
State number of reducers	carried on	board and	their fland	be rating and size
oute number of feddeets	carried on	bound und	then many	c raung and once

oute number of feddeets curret	a on bourd and then mange h
25.1	8/300 to 10/300
25.2	8/300 to 8/300
25.3	8/300 to 6/300
25.4	8/300 to 10/150
25.5	8/300 to 8/150
25.6	8/300 to 6/150
25.7	6/150 to 4/150
25.8	4/150 to 4/150
	4/150 to 3/150
	4/300 to 4/150
	6/300 to 4/150

#### **B26 MANIFOLD DERRICK/CRANE**

26.1	Is Manifold Derrick provided	no
26.2 26.3	Is Manifold Crane provided Is lifting equipment same port and starboard	yes no
26.4	If not give details State SWL at maximum outreach	1 midship SWL 5 tons